| A   |  | Reg. No. :             |                            |        |      |                            |               |       |               |        |       |               |        |
|---|--|------------------------|----------------------------|--------|------|----------------------------|---------------|-------|---------------|--------|-------|---------------|--------|
|   | <b>Question Paper Code: 93904</b>  |                        |                            |        |      |                            |               |       |               |        |       |               |        |
|   | B.E./B.Tech. DEGREE EXAMINATION, DEC 2021  |                        |                            |        |      |                            |               |       |               |        |       |               |        |
|   | Third Semester   |                        |                            |        |      |                            |               |       |               |        |       |               |        |
|   | Chemical Engineering   |                        |                            |        |      |                            |               |       |               |        |       |               |        |
|   | 19UCH305- CHEMICAL PROCESS CALCULATIONS  |                        |                            |        |      |                            |               |       |               |        |       |               |        |
|   |  | (Regul                 | ation                      | 2019   | )    |                            |               |       |               |        |       |               |        |
| Dura  | Duration: Three hours Maximum: 100 Marks   |                        |                            |        |      |                            |               |       |               |        |       |               |        |
|   |  | Answer A               | LL Q                       | uesti  | ons  |                            |               |       |               |        |       |               |        |
|   |  | PART A - (10           | 0 x 1 =                    | = 10 ] | Mai  | rks)                       |               |       |               |        |       |               |        |
| 1.  | 1. A cylinder contains 8 gms of He, 40 gms of Ne and 80 gms of Ar. (Molecular weights of the components are 4, 20 and 40 respectively) How many moles of He are there in the cylinder? |                        |                            |        |      |                            |               |       |               | CO     | 2- AP |               |        |
|   | (a) 1  | (b) 2                  |                            |        | (c)  | 4                          |               |       | (d            | ) 6    |       |               |        |
| 2.  | Which of the following term does not involve in ideal gas law?   |                        |                            |        |      |                            |               |       |               |        | С     | 01 <b>-</b> U |        |
|   | (a) Pressure   | (b) Volume.            |                            | (c) Te | emp  | eratu                      | ire           |       | (d)           | ) Tim  | e     |               |        |
| 3.  | Concept of material ba   | lance based upon?      | 1? CO                      |        |      |                            |               |       | 01 <b>-</b> U |        |       |               |        |
|   | (a) Conservation of mass (b) (   |                        |                            |        |      | (b) Conservation of energy |               |       |               |        |       |               |        |
|   | (c) Conservation of mo   | omentum                | (d) Conservation of Volume |        |      |                            |               |       |               |        |       |               |        |
| 4. A is one in which material enters and leaves the system CC without interruption. |  |                        |                            |        |      |                            | 01 <b>-</b> U |       |               |        |       |               |        |
|   | (a) Continuous process   | 3                      |                            | (b) B  | atc  | h pro                      | cess          |       |               |        |       |               |        |
|   | (c) Semi-batch process   | 3                      |                            | (d) N  | lone | e of t                     | he me         | entio | ned           |        |       |               |        |
| 5. In humidification the gas is in the liquid for the mass transfer to take part.   |  |                        |                            |        | fer  |                            |               | CO3   | - Ana         |        |       |               |        |
|   | (a) Soluble  | (b) Insoluble          |                            | (c) Pa | rtia | lly so                     | oluble        | e     | (d)           | ) Iner | t     |               |        |
| 6.  | During humidification  | process the dry bulb t | emper                      | ature  |      |                            |               | -     |               |        |       | CO2           | - App  |
|   | (a) increases  | (b) decreases          | (c                         | ) tend | s to | zero                       | )             |       |               | (d) re | emai  | ns the        | e same |

| /. Change in the internal energy for a steady-state system is alway | 7. | Change | in | the | internal | energy | for | а | steady-state | system | is | always |
|---|----|--------|----|-----|----------|--------|-----|---|--------------|--------|----|--------|
|---|----|--------|----|-----|----------|--------|-----|---|--------------|--------|----|--------|

CO1- R

|     |  | · · · · · · · · · · · · · · · · · · ·   |  |  |   |           |         |  |  |
|-----|--|---|--|--|---|-----------|---------|--|--|
|     | (a)  | a) Positive (b) Negative (c) Zero (d) None of   |  | of the menti   | of the mentioned  |           |         |  |  |
| 8.  | Hea<br>wha   | at of formations of at is the heat of reac  | A, B, C, and D, are 5<br>etion A + 4B -> 3C + I  | J, 10 J, 15 J, and 20<br>D?  | J respectively  | ', C      | O3- Ana |  |  |
|     | (a)  | 10 J  | (b) 20 J   | (c) 35 J   | (d)   | 45 J      |         |  |  |
| 9.  | In p<br>the  | presence of which g<br>form of heat?  | as is the fuel burnt to  | generate energy in   |   |           | CO1- U  |  |  |
|     | (a)  | Oxygen  | (b) Hydrogen   | (c) Methane  | (d)   | Nitrogen  |         |  |  |
| 10. | The  | e process of burning  | g fuels in the presence  | of oxygen is called  |   |           | CO1- R  |  |  |
|     | (a)  | Induction   | (b) Ignition   | (c) Condensati   | ion (d)   | Combustic | on      |  |  |
|     |  |   | PART – B (S  | 5 x 2= 10 Marks)   |   |           |         |  |  |
| 11. | 2 lita<br>H <sub>2</sub> Se  | res of NH, at 303 k<br>O <sub>4</sub> ,. Find the norma   | K (30°C) and 20.265 k<br>lity of the acid  | kPa is neutralised by  | 135 ml of solu  | ition of  | СО4- Е  |  |  |
| 12. | What is the purpose of doing mass balance for a chemical process? CO1- R |   |  |  |   |           |         |  |  |
| 13. | State the term humidification. CO1- R                                    |   |  |  |   |           |         |  |  |
| 14. | Writ   | e the procedure for   | doing energy balance   | for a process  |   |           | CO1- R  |  |  |
| 15. | Wha  | t are the three types   | s of fuels available?  |  |   |           | CO1- R  |  |  |
|     |  |   | PART – C   | (5 x 16= 80 Marks  | )   |           |         |  |  |
| 16. | (a)  | A gaseous mixture<br>$CO_2 = 8\%$ , $CO = 1$<br>molecular weight<br>303 K (30°C) and                | has the following co<br>$14, O_2 = 6\%, H_2O = 1^{\circ}$<br>of the gas mixture and<br>101.325 kPa.                        | mposition by volume $\% N_2 = 66\%$ Calculat d (ii) Density of the g   | e : $CH_4 = 1 \%$<br>te (i) Average<br>gas mixture at   | CO2- Apj  | p (16)  |  |  |
|     |  |   | Or   |  |   |           |         |  |  |
|     | (b)  | The analysis of the $66\%$ , $CO2 = 30\%$ the gas and (b) d ( $30^{\circ}$ C).                      | e gas sample is given<br>, NH3 = 4% %Find (a<br>ensity of the gas at 2   | a below (on volume t<br>a) the average molecu<br>202.65 kPa g pressur  | (1200) (CH <sub>4</sub> - 1) (1200) ( | CO3- Ana  | a (16)  |  |  |
| 17. | (a)  | An evaporator is f<br>15% NaOH and re<br>is precipitated as c<br>45% NaOH, 2%<br>evaporated, (b) kg | Ted with 15000 kg/h o<br>est water. In the operatorystals. The thick liques<br>NaCl and rest w<br>/h salt precipitated, (c | f a solution containin<br>tion, water is evapora<br>for leaving the evaporater. Calculate: (a)<br>) kg/h thick liquor. | ng 10% NaCl,<br>tted and NaCl<br>rator contains<br>kg/h water   | CO2- Apj  | p (16)  |  |  |

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- (b) Ethylene oxide is produced by oxidation of ethylene. 100 kmol of CO2- App (16) ethylene are fed to a reactor and the product is found to contain 80 kmol ethylene oxide and 10 kmol CO2. Calculate: (a) the percent conversion of ethylene and (b) the percent yield of ethylene oxide
- 18. (a) The dry bulb temperature and dew point of ambient air were found to be CO2- App (16) 302 K (29°C) and 291 K (18°C) respectively. Barometer reads 100 kPa. Calculate: (a) the absolute molal humidity, (b) the absolute humidity, (c) the % RH, (d) the % saturation, (e) the humid heat and (f) the humid volume.

Data: Vapour pressure of water at 291 K = 2.0624 kPa.

Vapour pressure of water at 302 K = 4.004 kPa.

Or

- (b) The DB and WB temperatures on a particular day in Madurai are CO3- Ana (16) observed to be 308 K (35°C) and 299 K (26°C) respectively. Using the psychrometric chart, Find: (a) the absolute humidity (H), (b) % RH, (c) DP..
- 19. (a) Flue gases leaving the boiler stack at 523 K (250°C) have the following CO2- App (16) composition :  $CO_2 = 11.31\%$ ,  $H_2O = 13.04\%$ ,  $O_2 = 2.17\%$  and  $N_2 = 73.48\%$  (by volume) Calculate the heat lost in 1 kmol of gas mixture above 298 K (25°C), using the heat capacity data given below:  $Cn = a + bT + cT2 + dT^3 k I/(kmol K)$

| Cp – a +01 | $\pm c_1 z \pm a_1$ | , KJ/(KIIIOI.K) |  |
|------------|---------------------|-----------------|--|
|            |                     |                 |  |

| Gas              | a       | b x 10 <sup>3</sup> | c x 10 <sup>6</sup> | d x 10 <sup>9</sup> |  |  |  |
|------------------|---------|---------------------|---------------------|---------------------|--|--|--|
| H <sub>2</sub> O | 21.3655 | 64.2841             | - 41.0506           | 9.7999              |  |  |  |
| O <sub>2</sub>   | 26.0257 | 11.7551             | - 2.3426            | - 0.5623            |  |  |  |
| CO <sub>2</sub>  | 32.4921 | 0.0796              | 13.2107             | -4.5474             |  |  |  |
| N <sub>2</sub>   | 29.5909 | - 5.141             | 13.1829             | -4.968              |  |  |  |
| Or               |         |                     |                     |                     |  |  |  |

(b) A stream flowing at a rate of 10000 mol/h containing 25 mole % N2 and

CO4- E (16)

75 mole % H, is to be heated from 323 K (50°C) to 493 K (220°C). Calculate the heat that must be transferred using Cp data given below:  $Cp = a + bT + cT^2 + dT^3$ , kJ/(kmol-K)

| Gas            | a       | b x 10 <sup>3</sup> | c x 10 <sup>6</sup> | d x 10 <sup>9</sup> |
|----------------|---------|---------------------|---------------------|---------------------|
| N <sub>2</sub> | 29.5909 | - 5.41              | 13.1829             | -4.968              |
| H <sub>2</sub> | 28.6105 | 1.0194              | -0.1476             | 0.769               |

- 20. (a) The ultimate analysis of coal sample is given below: Carbon : 61.5%, CO2- App (16) hydrogen : 3.5%, sulphur : 0.4%, ash : 14.2%, nitrogen : 1.8% and rest oxygen. Calculate :
  - (a) Theoretical oxygen requirement per unit weight of coal.
  - (b) Theoretical dry air requirement per unit weight of coal, and
  - (c) The Orsat analysis of flue gases when coal is burned with 90% excess dry air.

## Or

(b) The GHV (gross heating value) of gaseous n-butane is 2877.40 kJ/mol at CO2- App (16) 298 K (25°C).
Calculate its NHV (net heating value) in kJ/mol and kJ/kg. = 2442.5 kJ/kg. Latent heat of water vapour at 298 K (25°C)