# **Question Paper Code: 56902A**

#### B.E./B.Tech. DEGREE EXAMINATION, AUGUST 2021

#### Sixth Semester

#### **Chemical Engineering**

## 15UCH602 - CHEMICAL REACTION ENGINEERING-I

# (Regulation 2015) PART – A (10 X 2 =20 Marks) ANSWER ANY TEN QUESTIONS

1.	Difference between elementary and non-elementary reactions.	R	CO1
2.	Define rate of reaction.	R	CO1
3.	List out the methods that are used to analyse the kinetic data	U	CO1
4.	What situations recycle reactors are used?	Ap	CO2
5.	Give the size comparison equation for an n <sup>th</sup> order reaction.	U	CO2
6.	Justify what happens to the conversion when CSTRS connected in parallel	U	CO2
7.	Define yield and selectivity.	U	CO3
8.	What are parallel reactions? give examples	R	CO3
9.	Give the expression for overall fractional yield for N mixed flow reactors in series	U	CO3
10.	Why optimum progression should be known for a reaction?	R	CO4
11.	Compute $K_y$ at 10 atm if $K_p$ at this pressure is 0.00381 atm <sup>-1</sup> for the ammonia synthesis reaction from hydrogen and nitrogen at 500 ° C	Ap	CO4
12.	Define optimum temperature progression.	R	CO4
13.	On what aspects a non ideal flow will occur in the reactor – Explain?	R	CO5

- 14. List out the characteristics of tracer.
- 15. What is meant by C curve?

## PART – B (3 X 10 =30 Marks) ANSWER ANY THREE QUESTIONS

- 1 Determine an expression for rate of reaction interms of concentration and conversion for first order reaction using integral method of analysis. AP CO1
- A liquid phase reaction with stoichiometry A→R is carried out in a plug flow reactor whose rate versus concentration data is given below is studied. Determine the size of the plug flow reactor required to achieve 80% conversion of a feed stream of 1000 mol A/hr at C<sub>AO</sub>= 1.5 mol/l

C <sub>A</sub> ,	0.1	0.2	0.3	0.4	0.5	0.6	0.7	0.8	1.0	1.3	2.0
mol/l											
-r <sub>A,</sub>	0.1	0.3	0.5	0.6	0.5	0.25	0.10	0.06	0.05	0.045	0.042
(mol/l											
.min)											

3 Reactant A in the liquid phase reacts to produce R and S by the following reactions in parallel:

 $A \rightarrow R$ 

$$A \rightarrow S$$
 AP CO3  
rst order. A feed with  $C_{AO} = 1$ ,  $C_{PO} = 0$  and  $C_{SO} = 0$  enters in two mixed

Both these reactions of first order. A feed with  $C_{AO}=1$ ,  $C_{RO}=0$  and  $C_{SO}=0$  enters in two mixed flow reactors ( $\tau 1 = 2 \text{ min}$  and  $\tau 2=5 \text{ min}$ ) the composition within the first reactor is  $C_{A1}=0.40$ ,  $C_{R1}=0.40$  and  $C_{S1}=0.2$  find the composition of exit stream from the second reactor.

4 The first order irreversible liquid phase reaction is carried out in a mixed flow reactor. The density of the reaction mixture is  $1.2g/cm^3$  and the specific heat is 0.9cal/g.c. the volumetric flow rate is 200 cm<sup>3</sup>/s and the reactor volume is 10lit.  $k = 1.8 \times 10^5 e^{-12000/RT}$ . If the heat of reaction is -46000cal/mol and feed temperature is 293k (20°C). What are possible temperature and pressure for stable, adiabatic operation for a feed concentration of 4mol/lit.

CO4

Ap

CO<sub>5</sub>

U

R

5 Derive the equation for residence time distribution in mixed flow reactor. U CO5