A		Reg. No. :												
		Ouestion	Par	oer	Co	de:	U5′	701	7					
B.E./B.Tech. DEGREE EXAMINATION, APRIL 2024														
Fifth Semester														
		Mechan	ical E	ngi	neeri	ng								
		21UME501 – HE	AT A	ND	MA	SS 1	RA	NSFI	ER					
		(Re	gulat	ions	202	1)								
Dur	ation: Three hours								Μ	[axin	num:	100	Mar	ks
		Answ	er AL	LLQ	)uest	tions								
		PART A	- (10	x 1	= 10	Mar	·ks)							
1.	Planck's law is appl	licable to											CO	01 <b>-</b> U
	(a) Radiation from l	olack body				(b) N	lono	chro	mati	c rac	liatio	n		
	(c) Radiation of any	length				(d) A	ll of	the	abov	e				
2.	The Nusselt number	is a function of											CO	01 <b>-</b> U
	(a) Prandtl Number					(b) C	irash	off's	s Nui	nber				
	(c) Prandtl Number	And Grashoff's Nu	ımbeı	ſ		(d) N	Iach	Nur	nber					
3.							CO	01 <b>-</b> U						
	(a) Mach	(b) Frodue		(c	) Nu	sselt				(d) ]	None	e of t	he al	oove
4.	Weather is a examp	le of											CO	01 <b>-</b> U
	(a) Conduction curr	ent				(b) C	Conve	ectio	n cu	rrent				
	(c) Radiation curren	nt				(d) N	lone	of th	nese					
5.	The radiation emitted by a black body is known a			n as	us (						CO	)1 <b>-</b> U		
	(a) Black radiation	(b) Full radia	ation	(0	c) To	tal ra	adiat	ion		(	d) A	ll of	these	2
6.	The value of the wa	velength for maxir	num	emi	ssive	e pov	ver is	s giv	en by	/			CO	)1- U
	(a) Wien's law	(b) Planck	c's lav	V	(	c) St	efan	's lav	V		(d	) Foi	urier'	s law
7.	Drop wise condensation occurs on asurface C							CO	01 <b>-</b> U					
	(a) oily	(b) smoot	th			(c) g	lazed	1			(d	) coated		

8.	The multi-pass heat exchange	CO1- U						
	(a) To obtain high heat trans	sfer coefficient	(b) to reduce pressure drop					
	(c) to get a compact unit		(d) all of the above					
9.	Diffusion coefficient unit is			CO1- U				
	(a) m	(b) m/s	(c) s	(d) $m^2/s$				
10.	Number can be use	CO1- U						
	(a) Mach	(b) Sherwood	(c) Nusseh	(d) None of the above				
PART - B (5 x 2 = 10 Marks)								
11.	Summarize fin efficiency and fin effectiveness							
12.	Discuss heat transfer coefficient for natural convection is much lesser C							
	Than that for forced convec	tion?						
13.	List out any two shape facto	CO1- U						
14.	Show the heat flux curve fo	CO1- U						
15.	Show the anology of Heat transfer.							
$PART - C (5 \times 16 = 80 Marks)$								

16. (a) A iron plate (k = 60 W/m C, c =0.46 kJ/Kg. K,  $\rho$  = 7850 kg/m3 and CO2-App (16)  $\alpha$  = 1.6 x 10<sup>-5</sup>m<sup>2</sup>/s) of 50 mm thickness is initially at 225<sup>0</sup> C. Suddenly, both surfaces are exposed to an ambient temperature of 25<sup>0</sup> C with a heat transfer coefficient of 500 W/ m2 K. Calculate (a) the centre temperature at 2 min after the start of cooling (b) the temperature at a depth 1 cm from the surface at 2 min after the start of cooling and (c) the energy removed from the plate per sq.m during this time.

## Or

(b) A heating unit made in the form of a cylinder is 6mm diameter & CO2-App (16) 1.2m long. It is provided with 20 longitudinal fins 3mm thick which protrude 50mm from the surface of the cylinder. The temperature at the base of the fin is  $800^{\circ}$  C. The ambient temperature is  $250^{\circ}$ C. The film heat transfer co-efficient from the cylinder and fins to the surrounding air is  $10 \text{ W/m}^2$ k. Calculate the rate of heat transfer from the finned wall to the surrounding. Take k= 90W/mk.

17. (a) Air at 25°C flows over 1 m x 3 m (3 m long) horizontal plate CO2- App (16) maintained at 200°C at 10 m/s. Calculate the average heat transfer coefficients for both laminar and turbulent regions. Take Re (critical) = 3.5x105.insulation.

## Or

- (b) Examine the heat transfer from a 60 W incandescent bulb at 115°C CO2- App (16) to ambient air at 25°C. Assume the bulb as a sphere of 50mm diameter. Also find the % of power lost by free convection.
- 18. (a) A pipe carrying steam having an outside diameter of 20cm runs in a CO2 -App (16) large room, and is exposed to air at a temperature of 30°C. The pipe surface temperature is 200°C. Find the heat loss per meter length of the pipe by convection and radiation taking the emissivity of the pipe surface as 0.8.

## Or

- (b) Emissivity of two large parallel plates maintained at 800 °C and CO2 -App (16) 300°C are 0.3 and 0.5 respectively. Find net radiation net radiant heat exchange per square meter for these plates. Find the percentage reduction in heat transfer when a polished aluminium radiation shield of emissivity 0.06 is placed between them. Also find temperature of the shield
- 19. (a) The outer surface of the vertical tube, which is 1 m long and has an CO3 -App (16) outer diameter of 80 mm, is exposed to saturated steam at atmospheric pressure and is maintained at 50°C by the flow of cool water through the tube. What is the rate of heat transfer to coolant and what is the rate at which the steam is condensed at the surface.

## Or

(b) Hot exhaust gases which enter the cross flow heat exchanger at CO3 -App (16) 300°C and leaves at 100°C are used to heat water at a flow rate of 1 kg/s from 35°C to 125°C. The specific heat of the gas is 1000 J/ kg K. And the overall heat transfer coefficient based on the gas side surface is 100 W/m<sup>2</sup>K. Find the required gas side surface area using the NTU method and LMTD method

20. (a) Air at 1 atm and 25° C containing small quantities of iodine, flows CO3- App (16) with a velocity of 6.2 m/s inside a 35 mm diameter tube. Calculate the mass transfer coefficient for iodine. The thermo physical properties of air are: V=15.5 x 10-6 m<sup>2</sup>/s; D=0.82 x 10-5 m<sup>2</sup>/s.

(b) Air at  $20^{\circ}C(D=4.166*10-5 \text{ m}^2/\text{sec})$  flows over a tray length = CO3- App (16) 320mm and width = 420mm full of water with a velocity of 2.8m/sec. the total pressure of moving air is 1 atm pressure and partial pressure of water present in the air is 0.0068 bar. If the temperature on the water surface is  $15^{\circ}C$ . Calculate the evaporation rate of water.

Or