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A		Reg. No. :									
Question Paper Code: 97902											
B.E./B.Tech. DEGREE EXAMINATION, APRIL 2024											
Seventh Semester											
	Chemical Engineering										
19UCH702 - TRANSPORT PHENOMENA											
(Regulations 2019)											
Duration: Three hours Maximum:									ım: 1	00 Marks	
Answer ALL Questions											
PART A - $(10 \text{ x } 1 = 10 \text{ Marks})$											
1.	Tooth paste is an exan	nple of									CO1- F
	(a) Newtonian fluid	(b) Dilatant	(c)]	Bingh	am		(d) P	seud	o pla	stic
2.	Power law model is al	so called as									CO1- F
	(a) Bingham model	(b) Oswald-de Waale model									
	(c) Eyring model	(d) The Ellis model									
3.	$DV\rho/\mu$ is called										CO2- F
	(a) Grashoff number) Grashoff number (b) pradntl number (c) Reynolds number (d) Nusselt								Number	
4.	For laminar flow Reynolds number is								CO2- F		
	(a) $N_{Re} = 2100$	(b) $N_{Re} < 2100$	(c) I	$N_{Re} > 2$	2100				(d)	N _{Re} 2	>4000
5.	Sun is the finest example	ple of									CO3- F
	(a) Convection		(b)]	heat f	lux						
	(c) radiation		(d)]	Fissio	n.						
6.	The ratio of driving force and resistance is called										CO3- F
	(a) Force	(b) Flux	(c) s	shear	stres	S			(d)	shea	r rate
7.	What is the unit of diff	fusion coefficient?									CO4- F
	(a) m^2 .	(b) s	(c)	$m^2 s$	5.			(d	l) m	$^{2}/s.$	
8.	Diffusion of component	nts between the phase	s at eq	uilibr	ium	is					CO4- F
	(a) Zero (b) Infi	inity (c) Change	s conti	nuous	sly	(d)) Di	ffusio	on ne	ever	occurs

9.	Consider the above problem, estimate the value of Reynolds numbered							(CO5- R		
	(a) (0.12 (b) 0.13 (c) 0.14					(d) 0.15				
10.	The	fundamental law us	sed for mor	nentum tra	ansfer i	S			(CO5- R	
	(a) Fourier's law (b) Fick's law (c) Newtons's law (d) Erying n							nodel			
PART - B (5 x 2= 10 Marks)											
11.	Define Viscosity.							CO1- U			
12.	What is No slip condition?							(CO2- U		
13.	Define Conduction.							(CO3- U		
14.	Define Fick's law of diffusion						(CO4- U			
15.	State the Reynold's analogy.						(CO5- R			
	PART – C (5 x 16= 80 Marks)										
16.	(a)	Explain the theory o	of viscosity	of liquids.					CO1- U	(16)	
	Or (b) Compute the mean molecular velocity \hat{U} , cm sec ⁻¹ , and the mean free CO1- E (16) path $\hat{\lambda}$ of O ₂ at 1 atm and 273.2 ⁰ K. Assume d = 3 .0 A. what is the ratio of mean free path to the molecular diameter in this situation? Data: K= 1.38 X 10 ⁻¹⁶ erg/mol.K N= 6.023 X 10 ²³ l/gm mole n = Flow behavior index= 2.68 x 10 ¹⁵								(16)		
17.	(a)	Derive Navier-Stol	kes equatio	on by equa Or	tion of	motic	on.		CO2- App	(16)	
	(b) Find the equation for an average velocity of an incompressible fluid flowing in an annular region in two co-axial circular cylinder. Assume that the flow is laminar.					CO2 - App (16)					
18.	 (a) Calculate the heat loss per m² of surface area for an insulating wall composed of 25.4 mm thick fibre insulating board, where the inside temperature is 352.7 K and the outside temperature is 297.1 K. the thermal conductivity of fibre is 0.0048 W/m.K. 						CO3- App	(16)			

- (b) A thick walled cylindrical tubing of hard rubber having an inside CO3- App (16) radius of 5mm and outside radius of 20 mm is being used as temporary cooling coil in a bath. Ice water is flowing rapidly inside, and the inside wall temperature is 274.9 K. The outside surface temperature is 297.1 K. A total of 14.65 W. heat must be removed from the bath by the cooling coil. How many m of tubing are needed? The thermal conductivity is 0.151W/m.K.
- 19. (a) The O₂ (a) is diffusing through CO(B) under standard conditions CO4- App (16) with CO non diffusing. The total pressure is $1 \times 10^5 \text{ N/m}^2$ and temperature is 0°c. The partial pressure of O₂ at two planes, 2.0 mm apart is 1300 and 6500 N/m2. The diffusivity of oxygen in CO is $D_{AB} = 1.87 \times 10^{-5} \text{m}^2/\text{sec}$. Calculate the rate of diffusion of O₂ in kmole/m².sec.

Or

- (b) The solute HCl (A) is diffusing through a thin film of water (B) 2.0 CO4- App (16) mm thick at 283^{0} K. The concentration of HCl at point (1) at one boundary of the film is 12 wt. % HCl ($\rho 1 = 1061 \text{ kg/m}^{3}$) and the other boundary at point (2) is 6 wt % HCl ($\rho 2=1030 \text{ kg/m}^{3}$). The diffusion co. efficient of HCl in water is 2.5 x 10 ⁻⁹ m2/sec. Assuming steady state conditions prevail and the boundary is impermeable to water, calculate the flux of HCl in Kmole/m².sec.
- 20. (a) Arrive the equation $W'_{A}=WL_{c}A_{o}\sqrt{4}D_{AB}$ $V_{max}/\pi L$ for forced CO5- App (16) convection in falling liquid film.

Or

(b) Explain in detail about diffusion in laminar falling film. CO5- U (16)