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**Question Paper Code:55903**

B.E./B.Tech. DEGREE EXAMINATION, NOV 2019

Fifth Semester

Chemical Engineering

15UCH503-HEAT TRANSFER

(Use of HMT data book is permitted)

(Regulation 2015)

Duration: Three hours

Maximum: 100 Marks

Answer ALL Questions

PART A - (10 x 1 = 10 Marks)

1. Thermal conductivity is maximum for which substance ? CO1- R  
(a) Silver (b) Ice (c) Aluminum (d) Diamond
2. Heat transfer takes place according to \_\_\_\_\_ law of thermodynamics CO1- R  
(a) First (b) Second (c) Third (d) Zeroth
3. The ratio of energy transferred by convection to that by conduction is called CO2- R  
(a) Stanton number (b) Nusselt number (c) Biot number (d) Reynolds number
4. In forced convection, Nusselt number is function of \_\_\_\_\_ CO2- R  
(a) Grashoff number and Peclet number (b) Reynolds number and Prandtl number  
(c) Grashoff number and Prandtl number (d) Reynolds number and Grashoff number
5. The body which absorbs all radiations incident upon it is called as \_\_\_\_\_ CO3- R  
(a) Black body (b) White body (c) Opaque body (d) Transparent body
6. The Stefan Boltzman law states that \_\_\_\_\_ CO3- R  
(a)  $E \propto T$  (b)  $E \propto T^2$  (c)  $E \propto T^3$  (d)  $E \propto T^4$
7. In a shell and tube heat exchanger, baffles are provided on the shell side to CO4- U  
(a) Improve heat transfer (b) Provide support for tubes  
(c) Prevent stagnation of shell side fluid (d) All of the above
8. The convective coefficients for condensation usually lie in the range of CO4- R  
(a) 30-300 W/m<sup>2</sup> K (b) 60-3000 W/m<sup>2</sup> K (c) 300-10000 W/m<sup>2</sup> K (d) 2500-10000 W/m<sup>2</sup> K
9. In heat exchangers, the value of logarithmic mean temperature difference should be CO5- R  
(a) Maximum possible (b) Minimum possible (c) Zero (d) Constant

10. Heat is transferred from an insulated pipe to the surrounding still air mainly by \_\_\_\_\_ CO5- R  
(a) Conduction (b) Free convection (c) Forced convection (d) Radiation

PART – B (5 x 2= 10Marks)

11. Define thermal conductivity. CO1- R  
12. State Buckingham's  $\pi$  theorem. CO2- R  
13. List the applications of radiation shield. CO3- R  
14. Differentiate between film condensation and dropwise condensation. CO4- R  
15. Define effectiveness of a heat exchanger. CO5- R

PART – C (5 x 16= 80 Marks)

16. (a) A furnace wall consists of three layers. The inner layer of 10 cm CO1- App (16)  
thickness is made of firebrick ( $k = 1.04 \text{ W/mK}$ ). The intermediate layer of  
25 cm thickness is made of masonry brick ( $k = 0.69 \text{ W/mK}$ ) followed by  
a 5 cm thick concrete wall ( $k = 1.37 \text{ W/mK}$ ). When the furnace is in  
continuous operation the inner surface of the furnace is at  $800^\circ\text{C}$  while  
the outer concrete surface is at  $50^\circ\text{C}$ . Calculate the rate of heat loss per  
unit area of the wall, the temperature at the interface of the firebrick and  
masonry brick and the temperature at the interface of the masonry brick  
and concrete.

Or

- (b) A steel rod ( $K = 32 \text{ W/mC}$ ), 12 mm in diameter and 60 mm long, with an CO1- App (16)  
insulated end, is to be used as a spine. It is exposed to surroundings with  
a temperature of  $60^\circ\text{C}$  and a heat transfer coefficient of  $55 \text{ W/m}^2\text{C}$ . The  
temperature at the base of fin is  $95^\circ\text{C}$ .  
Determine  
(a) The fin efficiency  
(b) The temperature at the edge of the spine  
(c) The heat dissipation.

17. (a) Air at  $20^\circ\text{C}$  and pressure of 1 bar flowing over a flat plate at a velocity of CO2- App (16)  
3 m/s. If the plate 280 mm wide and at  $60^\circ\text{C}$ . Calculate the following  
quantities at  $x = 280 \text{ mm}$   
(i) Boundary layer thickness  
(ii) Local friction coefficient  
(iii) Average friction coefficient  
(iv) Thickness of thermal boundary layer  
(v) Local convective heat transfer coefficient  
(vi) Average convective heat transfer coefficient  
(vii) Rate of heat transfer by convection.

Or

- (b) Derive by dimension analysis,  $Nu = \phi(Gr, Pr)$  for free convection. CO2- App (16)

18. (a) (i) The sun emits maximum radiation at  $\lambda = 0.52 \mu$ . Assuming the sun to be a black body, calculate the surface temperature of the sun. Also calculate the monochromatic emissive power of the sun's surface. CO3 App (8)
- (ii) A furnace wall emits radiation at 2000 K. Treating it as black body radiation, calculate CO3 App (8)
- (1) Monochromatic radiant flux density at  $1 \mu\text{m}$  wave length.  
(2) Wave length at which emission is maximum and the corresponding emissive power.  
(3) Total emissive power.
- Or
- (b) A thin aluminum sheet with an emissivity of 0.1 on both sides is placed between two very large parallel plates that are maintained at uniform temperatures  $T_1=800 \text{ K}$  and  $T_2=500 \text{ K}$  and have emissivities  $\epsilon_1= 0.2$  and  $\epsilon_2 =0.7$  respectively. Determine the net rate of radiation heat transfer between the two plates per unit surface area of the plates and compare the result to without the shield. CO3- App (16)
19. (a) Classify the types of condensers and explain the working of any two type of condenser. CO4- U (16)
- Or
- (b) Explain with neat sketch about pool boiling curve for water. CO4- U (16)
20. (a) Explain the working of Shell and tube heat exchanger with neat diagram. CO5- U (16)
- Or
- (b) Hot oil with a capacity rate of  $2500 \text{ W/K}$  flows through a double pipe heat exchanger. It enters at  $360 \text{ }^\circ\text{C}$  and leaves at  $300 \text{ }^\circ\text{C}$ . Cold fluid enters at  $30 \text{ }^\circ\text{C}$  and leaves at  $200 \text{ }^\circ\text{C}$ . If the overall heat transfer coefficient is  $800 \text{ W/m}^2\text{K}$ , determine the heat exchanger area required for  
(1) Parallel flow  
(2) Counter flow CO5- U (16)

