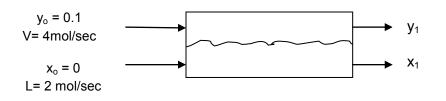
A		Reg. No. :										
		Question Paper	Code: 50	5901								
	B.E./B.Tech. DEGREE EXAMINATION, APRIL 2019											
	Sixth Semester											
	Chemical Engineering											
		15UCH601 - MAS	S TRANSF	ER - II								
		(Regulati	ion 2015)									
Dur	ation: Three hours				Maxim	um: 1	00 Marks					
		Answer AL	L Questions									
		PART A - (10 x	x = 10 Mat	rks)								
1.	The partial pressure of solute in the gas phase as the CO1- R process moves towards equilibrium.											
	(a) Increases	(b) Decreases	(c) Remain	s constant	(d)	Can'	t say					
2.	The operating line component will be a (a) Mole fraction	drawn in terms of linear. (b) Volume fraction		_		Weig	CO1- U					
3.		n column at total reflux.			(u)	Weigi	CO2- R					
5.	(a) 0	(b) ∞	(c) <1		(d) >	>1	C02- K					
4.	. ,	operated at			. ,	1	CO2- U					
	(a) 50	(b) 65	(c) 70			(d) 1	00					
5.		ned in the solid has the ow, then the tie lines on	-	•			CO3- U					
	(a) Are horizontal			(b) Are ve	ertical							
	(c) Pass through the	vertex representing 100	0% solid	(d) Are pa	arallel							

6.		n of oil seeds, which est rate of extraction	of the following forms of ?	the	CO3- U			
	(a) Whole seeds	(b) Broken seeds	(c) Flakes of the seeds	(d) None of the	above			
7.	Which of the follow effective dispersion	•	ormation of a stable and m	ore	CO4- U			
	(a) Low interfacial	tension	(b) Large density					
	(c) Low viscosity of	f the dispersed phase	e (d) Higher impell	er speed				
8.			C in two partially misc vity of separation at the p		CO4- U			
	(a) 1	(b) 0	(c) Infinite	(d) <1				
9.	A hollow – fibre me	embrane with isotrop	oic dense wall is suitable for	Dr	CO5- R			
	(a) Micro filtration	(b) Reverse osmos	sis (c) Pervaporation	(d) Electrodia	lysis			
10.	The metallic electrode which does not take part in the electrolytic CO5- reaction.							
	(a) Ni	(b) Fe	(c) Ag	(d) Cu				
		PART – B	(5 x 2= 10 Marks)					
11.	Distinguish between	n Raoult's law and H	· /		CO1- U			
12.	At 350K the vapou and 35kPa respecti	r pressures of the p ively. The mixture phase mole fraction	toluene contains 20 mole% oure benzene and toluene follows Raoult's law. Es on of benzene in contact	are 92kPa timate the	CO2- U			
13.	What is selectivity i	n extraction operation	on?		CO3- U			
14.	Define heap leachin	ıg.			CO4- U			
15.	How pressure swing	g adsorption is facili	tated?		CO5- U			

PART – C (5 x 16= 80 Marks)

16. (a) (i) Define the term number of transfer unit and develop the CO1-U (10) expression to calculate height of the packed column?

(ii) Water is used to absorb ammonia from a gas mixture in a single CO1- U
(6) separation stage contactor. The process is schematically represented in the figure



The inert gas and liquid flow rates, and the inlet mole ratios are given in the figure. If the exit liquid stream contains 0.08 moles of ammonia,

(i) Develop the equilibrium relation between Y and X.

(ii) If the stage efficiency is 50% what would be the outlet gas and liquid compositions.

Or

(b) (i) A gas is absorbed in water using a packed tower. The CO1-U (8) equilibrium relationship may be taken as $Y_e = 0.06 X_e$ where Y_e and X_e are ratios of moles of solute to moles of inert component. The terminal conditions are: soluble

	Тор	Bottom
Х	0	0.08
Y	0.001	0.009

- (ii) List the factors to be considered during the selection of CO1- U (8) absorbent.
- 17. (a) A feed mixture containing equimolar quantities of A and B is CO2-E (16) distilled differentially such that 60 mole% of the feed is distilled out. Estimate the composition of the residue and distillate. Equilibrium data:

XA	0	0.1	0.2	0.3	0.4	0.5	0.6	0.7	0.8	0.9
УA	0	0.21	0.38	0.51	0.63	0.72	0.78	0.85	0.91	0.96
XA	0	0.1	0.2	0.3	0.4	0.5	0.6	0.7	0.8	0.9
УA	0	0.21	0.38	0.51	0.63	0.72	0.78	0.85	0.91	0.96

(b) A bubble-cap fractionating column of 12 plates working at an CO2-E (16) average efficiency of 75% is being used to distill 1000 kg/hr of aqueous methanol at its bubble point enters the tower. The feed, overhead product and bottom product are 50 mole%, 90 mole% and 10 mole% methanol respectively. A total condenser is placed at the top of the column. The reflux is sent at its bubble point. If the reflux ratio is 1.7 times the minimum value, test whether the column available is satisfactory. The VLE data are:

Mole % of methanol in liquid	8	10	20	30	40	50	70	80	90
Mole % of methanol in vapour	36.5	41.8	57.9	66.5	72.9	77.8	87	95.8	97.9

18. (a) Explain working principle of the mechanically agitated and CO3-U (16) centrifugal extractors with neat sketch.

Or

(b) A solution containing 18 wt% acetone in water is to be extracted CO3-U (16) with pure monochlorobenzene by countercurrent extraction process. Monochlorobenzene and water are immiscible in the operating conditions. Estimate the percentage of extraction and weights of final raffinate and extract.

X' kg acetone/kg water	0.0258	0.0739	0.1658	0.267	
Y' kg acetone/ kg	0.0288	0.0704	0 1560	0.237	
monochlorobenzene	0.0200	0.0704	0.1500	0.237	

19. (a) (i) Sketch the typical equilibrium diagram of leaching operation. CO4- U (2)

(ii) 2.3 Kg/s of solid containing 0.55 Kg/s soluble material is to be CO4-U (14) washed with 2.8 Kg/s pure solvent in a counter – current unit. The final residue is to contain not more than 0.1% solute when dried. Find the number of stages given that the amount of solution in under flow varies with solute concentration according to the relation: W = 0.2 X + 0.3, Also find the concentration and quantities in and out from each stage

(b) A vegetable seed material containing 0.4 kg oil/kg insoluble solid CO4-U (16) is washed with hydrocarbon solvent in order to recover 90% of the oil in a counter current unit. It is found that the under flow varies with the concentration of classifier as given below. If the solvent input flow 0.5 kg/kg insoluble solid. Find the number of stages required?

Kg solution / kg insoluble solid	0.3	0.32	0.34	0.36	0.38	0.4
Kg solute / kg solution	0	0.1	0.2	0.3	0.4	0.5

20. (a) (i) Why did we not take osmotic pressure in account for CO5-U (4) microfiltration and ultra filtration?

(ii) Explain the method of estimating the retention and CO5-U (4) permeability of membrane.

(iii) Differentiate between single stage and multistage reverse CO5-U (8) osmosis process with neat sketch.

Or

(b) (i) Justify that for cross current two-stage treatment of liquid CO5-U (8) solution by contact filtration, when the adsorption isotherm is linear, the least total adsorbent results if the amounts used in each stage are equal.

(ii) Explain the principles of ion exchange process. CO5- U (8)